

Amendments to Specification

1. Applicant submits a paragraph to be added as the first paragraph of page 1 of the specification. The paragraph inserts the reference to a prior filed PCT and provisional applications from which priority is claimed.

The new paragraph is as follows:

This application is the U.S. National Stage Application under 35 U.S.C. 371 of PCT Application No. PCT/US2004/013669 filed 29 April 2004 and published 18 November 2004 under International Publication No. WO 2004/099090. This application claims benefit of U.S. Provisional Application No. 60/466,794 filed 01 May 2003 and PCT Application No. PCT/US2004/013669.

2. The Applicant submits the following replacement paragraph amending the specification, the original paragraph begins on page 8, line 6 of the specification.

The amendment adds the words "flow rate" to line 9. This language was inadvertently omitted in the original application.

The replacement paragraph beginning page 8, line 6 is as follows:

Within the filter influent channels 24a-24h the conversion agent or conversion agent-clean water mixture is mixed with the wastewater and the resulting mixture is transferred to the filter channel 42. The influent flow rate to the selected filter unit(s) is reduced. The denitrification influent flow can vary and is known in the art. Typically, the flow rate of fluid through the filter influent piping 30a-30h is reduced during the denitrification process. However, under certain conditions, the flow rate can remain the same, depending on the denitrification loading

relative to the TSS (total suspended solids) and particle size distribution. In a non-limiting example, during the normal filtration mode, the flow rate through the filter influent piping 30a-30h is approximately 8 gallons/min/ft<sup>2</sup> (328.98 L/min/m<sup>2</sup>) whereas in a denitrification mode the flow rate is reduced to approximately 2.6 gallons/min/ft<sup>2</sup> (106.92 L/min/m<sup>2</sup>.) After flowing to the filter channel 42, the wastewater-methanol mixture accumulates and rises before flowing over a second weir 42a into the filter unit 40. The denitrification phase continues until samples of treated wastewater indicate acceptable NO<sub>x</sub>-N levels. As described above, conveying the mixture of wastewater and conversion agent to the filter media containing the microorganisms initiates the denitrifying process. Furthermore, the present invention enables selective denitrification of at least one specific filter 40 within the filtration system 10 while simultaneously operating some or all of the remaining filters in the filtration mode (the remaining filters do not receive the conversion agent nor is the flow rate to these filters reduced.) This method provides the flexibility to continuously filter wastewater during a denitrification process, even during critical times such as peak wastewater operating loads, storm events, or phosphorus removal since the entire filter system does not have to be shut down or taken out of filtration mode.